Improvement of Pitting Corrosion Resistance of Type 430 Stainless Steel by Electrochemical Treatments in a Concentrated Nitric Acid

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Electrochemical surface treatments have been attempted in 5 kmol/m³ HNO₃ solution to improve pitting corrosion resistance of Type 430 stainless steel. Three different surface treatments were carried out for the same time period (2.9 h) under conditions of immersion, potentiostatic polarization at 0.9 V vs. Ag/AgCl/sat.KCl reference electrode (E=+0.222 V vs. SHE) and potential cycling between 0.6 and 0.9 V. The pitting corrosion resistance was evaluated by an ordinary pitting potential measurement and droplet tests which simulates atmospheric corrosion in marine environments. It was found that the potential cycling treatment is most effective among them to improve pitting corrosion resistance. The surface analysis by EPMA and XPS indicated that the potential cycling most successfully removes MnS inclusions and increases Cr content in the passive film.

KEY WORDS: passive film; MnS inclusions; pitting corrosion; stainless steel; potential cycling polarization; nitric acid.

1. Introduction

The development of high corrosion resistant stainless steel (SS) with adequate reliability is an indispensable factor for ensuring the safety and economical operation of power plants, reducing maintenance cost of harbor and other infrastructure expose in marine atmospheric environment. One of the most severe and destructive types of localized attack is pitting corrosion, especially on ferritic SS due to its low nickel content.

However, ferritic SS is being promoted to be used more widely owing to their moderate corrosion resistance and affordable cost. Similar trend was also reported by U.S Geological Survey, engineers have been encouraged to substituting low-nickel stainless steels for austenitic grades in construction applications in order to offset high and fluctuating nickel prices. Nickel-free specialty steels are sometimes used in place of stainless steel within the power-generating and petrochemical industries. Another report explained ferritic stainless steel has the characteristics that it does not include Ni, which is a problem due to metal allergies, and tends not to cause stress corrosion cracking, and so on. An extensive number of researches have been performed on the origin of pitting corrosion. It has been hypothesized that pitting corrosion is caused by aggressive species in solution, dissolution of inclusions due to low pH, Cr:Fe oxide film alteration, oxide film thickening or thinning, or surface/oxide contamination from sulfur or other species. It has been well reported that localized corrosion initiates in stainless steels at inclusions, in particular, MnS inclusions and many mechanisms of pit initiation at Mn(Fe,Cr)S inclusions have been proposed, but the basic mechanism is that either the inclusion begins to dissolve or the matrix around the inclusion dissolves, leading to the acid pitting mechanism. The low pH causes preferential dissolution of Mn(Fe,Cr)S inclusions, releasing sulfur species that are known to cause damage to oxide films by suppressing repassivation, as well as by initiating further Mn(Fe,Cr)S inclusion dissolution. 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Analyzing the potential of wider uses of ferritic SS in one hand and pitting corrosion’s threat to deteriorating the steel in another hand, led to an idea to increase the ferritic SS pitting corrosion resistance by surface passivation; in concentrated nitric acid is one of the options. The use of nitric acid as a cleaning and passivating reagent of stainless steels is commonly employed in industry. The strong oxidizing conditions favour the formation of a passive film on the parts, which led to the use of the term “passivation” to describe the above treatment. Passive film forms spontaneously on
stainless steels upon contact with air or with an electrolyte containing a sufficient amount of dissolved oxygen, so the purpose of prior immersion in HNO₃ solutions is to form a protective passive film and to remove the MnS inclusions from the surface.⁵.⁶ MnS inclusions have been well known as a preferential site of pitting. Therefore, in order to increase the pitting resistance, the formation of a denser passive film and MnS inclusions removal is necessary. For this purpose, 20–40 vol% HNO₃ (3–6 M) solutions are often used at temperatures ranging from ca. 20 to ca. 70°C. J. S. Noh et al.⁵ suggested that the use of 20–25 vol% of HNO₃ (3–4 M) has the most beneficial effect on improving pitting resistance. In addition, N. Padhy et al.⁶ analyzed the effect of nitric acid concentration on 304L SS ranging from 1 to 11.5 kmol/m³ and the results showed that the good passive film stability in 1 kmol/m³ and 4 kmol/m³ nitric acid. In 8 and 11.5 kmol/m³ nitric acid, breakdown of passive film was observed, and the surface was stained with corrosion product.

Another number of research groups also have done extensive research on the similar field. Barbosa⁶ investigated the pitting resistance of AISI 316 SS after passivation in diluted nitric acid and resulted an increasing of pitting potential under open circuit conditions in aerated sea water. It was suggested that immersion in the nitric acid solution was found to remove the sulphide inclusions from the metal surface. Similar results were also found by Noh et al.⁶.

There were a small number of publications on improvement of pitting corrosion resistance by the polarization methods. Ziad Bou-Saleh et al.⁶ found that simple cyclic linear potentiodynamic polarization technique as a method of improving corrosion properties of passive films formed on a biomedical-grade 316LVM surface in phosphate buffer. The results demonstrated that the modification between the potential of hydrogen and oxygen evolution results in the formation of a passive film that offers significantly increased corrosion resistance (both pitting and general) when compared to the naturally grown passive film. The increasing of cycle number and anodic potential limit improved corrosion resistance. Another research group investigated the formation of passive film by potential square-wave polarization in hot sulfuric acid bath and they succeeded to produce a thick passive film.³⁷,³⁸ These studies open more possibility to enhance the passive film properties by different type of electrochemical method. Accordingly, this research has aims to look for a method to increase pitting corrosion resistance of type 430 SS for marine atmospheric application by removal of MnS inclusions from surface safely and without leaving large pits behind will be investigated as well as formation of protective passive film.

2. Experimental

2.1. Materials and Specimens

Type 430 SS sheets were cut into 15 × 15 mm and then underwent to electrodeposition coating employing an organic resin, which was cured at 150°C for at least 1 200 s. This coating procedure was done in order to reduce the occurrence of crevice corrosion at the edge of the specimens. They were embedded in epoxy resin to give a two-dimensional surface and were ground with 1 000 grit before experiment. A conventional three electrode setup was employed, consisting of platinum counter electrode, a Ag/AgCl/sat.KCl reference electrode (SSC) and a working electrode of the stainless steel. The composition of the stainless steel is given in Table 1.

2.2. Surface Treatments

In order to reduce MnS inclusions on 430 SS surface, the surface treatment was carried out in an aerated 5 kmol/m³ HNO₃ solution (32%vol) by three different methods; (1) immersion, (2) potentiostatic polarization and (3) potential cycling. For the immersion treatment, the specimen was just submerged for 2.9 h in the solution. During the treatment, the corrosion potential change was measured to confirm the passivation process. The potentiostatic treatment was performed by polarizing the specimen at 0.9 V for 2.9 h. In order to dissolve more inclusions, the applied potential has been raised up to 0.9 V, right before onset potential of transpassive region. In Fig. 1, anodic polarization curve of 430 SS in 5 kmol/m³ HNO₃ solution at 25°C is shown. It can be seen that the transpassive dissolution of 430 SS starts above about 1.0 V in this solution. The potential cycling treatment was carried out by cyclic potential scans in the passive region between 0.6 and 0.9 V. The same result was plotted in log of Y-axis. The potential was positively scanned from 0.6 to 0.9 V at 10 mV/s and was quickly reversed to 0.6 V to reduce the treatment time. The potential cycling was carried out 350 times for 2.9 h. All electrochemical measurement was done at 25°C, unless otherwise noted.

2.3. Pitting Corrosion Tests

The pitting resistance was evaluated by two different droplet tests.³⁹–⁴¹ In their droplet tests, a droplet of 100 μL of 1 kmol/m³ MgCl₂ was placed on the sample surface at 25°C in a relative humidity (RH) programmable chamber. In the droplet test (I), the RH was step-wisely lowered from 95, 80, 75, 65, 55, 45 and 35%, as shown in Fig. 2. The exposure time at each RH was 4 days, where water molecule in

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Table 1. Chemical composition of Type 430 SS.

<table>
<thead>
<tr>
<th>Element</th>
<th>C</th>
<th>Si</th>
<th>P</th>
<th>S</th>
<th>Mn</th>
<th>Ni</th>
<th>Cr</th>
<th>Fe</th>
</tr>
</thead>
<tbody>
<tr>
<td>Mass%</td>
<td>0.081</td>
<td>0.52</td>
<td>0.033</td>
<td>0.006</td>
<td>0.31</td>
<td>0.12</td>
<td>16.2</td>
<td>Bal.</td>
</tr>
</tbody>
</table>

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Fig. 1. Anodic polarization curve of Type 430 stainless steel in 5 kmol/m³ HNO₃ solution at 25°C recorded at scan rate of 10 mV/s.
the droplet was in equilibrium with water vapor in the air.\textsuperscript{39,40} The equilibrium chloride concentrations at respective RHs are shown in Fig. 2.\textsuperscript{39} At the end of each RH, the surface was observed to check the pitting corrosion occurrence. In the droplet test (II), a droplet of 100 \(\mu\)L of 0.5 kmol/m\(^3\) NaCl solution was placed on the specimen surface. The sample was exposed to the wet-dry cycles shown in Fig. 3. To confirm the results of the droplet tests, the pitting potential (\(E_{\text{pit}}\)) was determined from anodic polarization curve measured at 10 mV/s in 0.5 kmol/m\(^3\) NaCl solution at 25\(^\circ\)C. The experimental setup was similar with that of the surface treatment.

### 2.4. Surface Characterization

Distribution of MnS inclusions on 430 SS surface before and after the surface treatments was investigated by a Scanning Electron Microscope (SEM) with Electron Probe Micro Analysis (EPMA). After the surface treatments, the specimens were cleaned in acetone and sonicated for 15 min and then dried up with N\(_2\) gas. The passive film was characterized with X-ray Photoelectron Spectrometer (XPS, JEOL JPS-9010MC). All binding energies given in this paper are relative to the Fermi level, and all spectra were excited with the Al K\(_\alpha\) line (1 486.61 eV). The used current and voltage for X-ray source were 10 mA and 10 kV, respectively. The binding energies were calibrated using the peak energy of C 1 s of contaminant carbon, 285.0 eV. The take-off angle defined as the angle between the direction of the photoelectron path to the electron spectrometer and the specimen surface was 90\(^\circ\). XPS measurement was performed with 2 modes; wide scan for qualitative analysis and narrow scan for a detailed measurement of each element of the major peak. It could distinguish the electron binding state of the component, whether as metal or as oxide and also calculating the quantitative analysis for the oxide film.

### 3. Results and Discussion

#### 3.1. Surface Treatments

The change in the rest potential \(E_{\text{rest}}\) of 430 SS in 5 kmol/m\(^3\) HNO\(_3\) solution is shown in Fig. 4. The \(E_{\text{rest}}\) shifts gradually in positive direction approximately from 0 to 0.15 V at 2.9 h. This indicates passivation progresses under the immersion treatment. Since it continues to shift positively, the passive film is still growing at 2.9 h. Noh et al.\textsuperscript{5} reported that for 304 SS, MnS dissolution occurs around 0.2 V with respect to SCE (E=+0.244 V vs. SHE) in 20 vol\% of nitric acid (approximately 3 kmol/m\(^3\)). Thus, 2.9 h-immersion treatment employed in this study may not be sufficient to remove MnS inclusions. A typical result of the potential cycling treatment in 5 kmol/m\(^3\) HNO\(_3\) solution at 25\(^\circ\)C is shown in Figs. 6(a)–6(b) and 7(a)–7(b) where only anodic scans from 0.6 to

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**Fig. 2.** Change of relative humidity in the droplet test (I). The RH was stepwisely dropped from 95 to 35% at at 25\(^\circ\)C. The \([\text{Cl}^-]\) indicates the equilibrium chloride concentration of the chloride solution droplets at each RH.

**Fig. 3.** Change of relative humidity (RH) and temperature (T) in the droplet test (II). The RH and T were cycled to simulate actual atmospheric environment.\textsuperscript{42}

**Fig. 4.** Change in rest potential of Type 430 stainless steel with time in 5 kmol/m\(^3\) HNO\(_3\) solution at 25\(^\circ\)C.

**Fig. 5.** Potentiostatic polarization of Type 430 stainless steel at 0.9 V in 5 kmol/m\(^3\) HNO\(_3\) solution at 25\(^\circ\)C.
0.9 V are presented. The cathodic scans from 0.9 to 0.6 V were not recorded because the potential was quickly reversed to reduce the time period of the surface treatment. On the first scan, the current density increases significantly with potential. This current is mainly due to the formation of passive films and anodic dissolution of the constituent metals. It may include current for dissolution of MnS. On the following scans, the magnitude of current density decreases and becomes lowered after 20 scans and does not much change until 350 scans. The magnitude of current density at 0.9 V of each scan at 25 and 50°C was summarized and shown in Fig. 8. Potential cycling at 50°C is slightly higher than that at 25°C from the first until the last scan (350). This discrepancy may have some contributions on the improvement of pitting corrosion of ferritic SS.

3.2. Evaluation of Pitting Corrosion Resistance

The pitting resistance was evaluated by the droplet tests. The results of the droplet test (I) shown in Fig. 2 are shown in Table 2. The RH and chloride concentration shown is the critical value of pitting occurrence. For example, pitting occurred at 80%RH ([Cl\(^-\)] = 4 kmol/m\(^3\)) for the as-polished sample. Above 80%RH (below 4 kmol/m\(^3\) [Cl\(^-\)]), no pitting occurred even if it was exposed for 100 h because the surface was completely passivated, but at 80% RH or below (4 kmol/m\(^3\) [Cl\(^-\)] or above), pitting would occurred.

As-polished sample suffered from pitting at 80%RH ([Cl\(^-\)] = 4 kmol/m\(^3\)) and the immersion and potentiostatic-treated samples at 65%RH ([Cl\(^-\)] = 6 kmol/m\(^3\)). The immersion and potentiostatic treated samples have slightly better pitting corrosion resistance than non-treated sample. A higher pitting corrosion resistance was obtained by the potential cycling of 350 scans which has a critical RH\(_{\text{critical}}\) and [Cl\(^-\)]\(_{\text{critical}}\) of 35% and 9.8 kmol/m\(^3\), respectively. The passivated surface could be kept from 4 kmol/m\(^3\) [Cl\(^-\)] to 6 kmol/m\(^3\) by the immersion and potentiostatic treatments and then to 9.8 kmol/m\(^3\) by the potential cycling. It was reported in the previous study that the [Cl\(^-\)]\(_{\text{critical}}\) and RH\(_{\text{critical}}\) for Type 304 SS are 6 kmol/m\(^3\) and 65% under the droplet test, respectively. The pitting corrosion resistance of 430 SS treated by the immersion and potentiostatic is equal with that of 304 SS. Furthermore, higher pitting corrosion resistance is expected by the potential cycling treatment.

However, in the droplet test (II) shown in Fig. 3, which may be a severer corrosion condition that the droplet test (I),
the sample treated by the potential cycling at 25°C could not stand from pitting after 1 cycle. A very good result was given by the sample of the potential cycling at 50°C. It did not suffer pitting after 4 cycles of wet and dry environment. Therefore, the potential cycling treatment at higher temperature is more effective.

Pitting corrosion potential $E_{\text{pit}}$ was measured in 0.5 kmol/m$^3$ NaCl solution at 25°C to confirm the results of the droplet tests. The results are shown in Fig. 9. The criteria to determine pitting corrosion potential is when the current has reached 100 $\mu$A/cm$^2$. The $E_{\text{pit}}$ values of the as-polished and immersion treatment are quite similar, around 0.25 V. The pitting corrosion resistance after the surface treatment increased from 0.30 to 0.45 of potentiostatic and 350 potential scans at 25°C, respectively. A very high pitting corrosion resistance was achieved by the potential cycling at 50°C. The $E_{\text{pit}}$ was 0.90 V which is just below the transpassive dissolution potential. The results of $E_{\text{pit}}$ measurements show good consistency with the droplet tests.

### 3.3. Surface Examination

SEM image of the treated 430 SS sample surface by the 350 potential cycling at 25°C is shown in Fig. 10. The micro pits with about 2 $\mu$m diameters were found on the surface which is the actual size of MnS inclusion. It is thought that the surface treatment removes the MnS inclusions successfully without dissolution of the substrate. Probably, the substrate quickly passivates just after MnS dissolution in nitric acid solution, unlike in chloride solutions. Elemental mappings in Fig. 11 showed the MnS inclusions at higher magnification. Fe and Cr are not incorporating with Mn and S, so the surrounding of MnS inclusion is not covered by protective chromium-enriched, leaving it exposed defenselessly to the corrosive environment.

In Fig. 12 shows the distribution of MnS inclusions. The number of MnS inclusions was much reduced by surface treatment. The number of potentiodynamic scan also affect on reducing the inclusions. More scans would dissolve more inclusions which means the preferential site of pitting is removed. The square dotted line (Fig. 12(b)) is a cluster of micro pits and its contains very little amount of Fe, but contains high concentration of Cr. This Cr enrichment enable pit to repassivate and inhibits the growth of the micro pit even during polarization in NaCl and droplet test either in equilibrium and wet-dry cycle environment. A small amount of Fe was dissolved out along with MnS inclusion. Accordingly, pitting resistance of 430 SS increased due to the removal of initiation sites of pitting, MnS inclusions and chromium enrichment.$^{6,43)}$

Figure 12(c) is the mapping of elements after surface treatment 350 cycles of PC at 50°C. Chromium covers larger area which is thought to be chromium carbide.$^{44)}$ Some undissolved MnS inclusions were also still remained, even though their size (around 1–2 $\mu$m) has exceeded the critical value of MnS inclusion to cause pitting.$^{33,45)}$ Probably because their location are adjacent to chromium carbide, so hindered the inclusion dissolution, even in extreme condition; wet-dry cycles. In other area, a small micro pit was found, that covered by Cr.

In Fig. 13, the ratio of Cr to Fe in the passive film obtained by X-Ray Photoelectron Spectroscopy (XPS) is
presented. The Cr/Fe ratio was 0.1 for the as-polished sample, 0.35 for the immersion treatment, 1.0 for the potentiostatic, 0.8 for the potential cycling at 25°C and 1.5 for the potential cycling at 50°C. The XPS study indicates the pretreatments improve the passive film, especially the potential cycling at 50°C.

3.4. Mechanism of the Pitting Resistance Improvement by Potential Cycling

The difference in the pitting corrosion resistance of 430 SS by different pretreatments; immersion, potentiostatic and potential cycling in concentrated nitric acid are discussed below.

Figure 14(a) is the schematics of MnS dissolution and passive film formation by the immersion treatment in concentrated nitric acid. Once the surface is exposed to the air, the air-formed passive film is formed on the surface. The MnS inclusions are distributed on the surface and less-protective passive film covers them because the MnS inclusions contain less Cr. Therefore, they become the weak point and pitting takes place preferentially at the inclusion sites. After the immersion in 5 kmol/m³ HNO₃ solution, the air-formed passive film turns to stable passive film in this solution. The Cr/Fe ratio of the passive film increases from 0.1 to 0.35 by XPS analysis. The MnS inclusions might not be electrochemically dissolved out from the report by Noh⁵ in which MnS dissolution in 20–25 vol% HNO₃ took place around 0.30–0.40 V vs SCE, although they might dissolve chemically¹⁴ according to the reaction;

\[ \text{MnS} + 2H^+ \rightarrow \text{Mn}^{2+} + H_2S \]

In Figs. 14(b)–14(c), the schematic of MnS dissolution and passive film formation under the conditions of the potentiostatic and potential cycling are displayed. In the initial stage, some inclusions dissolve out due to applied anodic potential. MnS inclusions are argued to decompose electrochemically at high potentials.¹⁸

\[ 2\text{MnS} + 3H_2O \rightarrow 2\text{Mn}^{2+} + S_2O_7^{2-} + 6H^+ + 8e^- \]

\[ \text{MnS} + 2H^+ \rightarrow \text{Mn}^{2+} + S + H_2 \]

The reactions above will occur in the anodic polarization, the remaining inclusions on the surface will be covered by a very thin passive film, which thought have different composition with that one formed on the substrate of SS. Finally, under the potentiostatic polarization at 0.9 V, the condition of the surface is similar with that of surface at the initial stage. The passive films consist of Cr and Fe in a balance composition, around 1.

The difference between the potentiostatic and potential cycling is the application of cathodic potential change in potential cycling. It takes place in very short time from 0.9 to 0.6 V; however the reduction of passive film thickness could occur,⁴⁶,⁴⁷ including the thin film that covered the inclusions, which might give opportunities for MnS to be dissolved out in the subsequent anodic scan. As a result more MnS inclusions are forced to remove from the surface, some by chemical dissolution and mostly by electrochemical. Running to the next scans, the same process will undergo. At last scan, 350, much thicker passive film with Cr enriched is formed stably on the surface and the number of
MnS are much reduced. Even though the thickness of passive film a little suppressed in cathodic scan, the accumulative thickness of anodic scan is sufficient to protect the surface from further dissolution, even during the atmospheric droplet tests where extreme condition of chloride ions occurred. The final stage of passivation by potential cycling results a higher ratio of chromium on iron, 1.5 (Fig. 13).

### 4. Conclusions

From results obtained with type 430 stainless steel subjected to potential cycling surface treatments in concentrated nitric acid, the following conclusions are drawn:

1. Micro pits with 1–2 μm diameters were found on the surface. Therefore, the employed method was successfully removed the inclusions and formed protective passive film.
2. After surface treatment, it was found chromium enrichment inside pit that enable the pit to repassivate and resists its growth.
3. Treated SUS 430 SS by potential cycling 350 scans at 50°C is suitable for applications in marine atmospheric environment as no pit propagates between 95 and 35% relative humidity ([Cl⁻] = 2 and 9.8 kmol/m³, respectively).

### REFERENCES